IN THE CLAIMS

Please amend the claims as follows:

Claim 1 (Currently Amended): A process for preparing hydrogen cyanide by autothermal noncatalytic oxidation of one or more nitrogenous hydrocarbons or a nitrogenous hydrocarbon mixture in which the wherein said nitrogenous hydrocarbons, an oxygen-containing gas, with or without ammonia, with or without water, with or without a gas eontaining comprising nitrogen oxides and with or without other essentially inert feed gas constituents are introduced into a flame reaction zone, react in the flame reaction zone and a post-reaction zone at a temperature of from 1000 to 1800°C for a reaction time of 0.03 to 0.3 s to form a cleavage gas which comprises at least the constituents hydrogen cyanide, carbon oxides, hydrogen, water, ammonia, nitrogen, light hydrocarbons with or without other cleavage gas constituents, the atomic C/N ratio in the reaction zones being from 1 to 7 and the atomic air ratio λ_{ato} being <0.6, the said cleavage gas being cooled and separated.

Claim 2 (Currently Amended): A process as claimed in claim 1, wherein <u>said</u> ammonia is introduced into the said flame reaction zone.

Claim 3 (Currently Amended): A process as claimed in claim 1-or-2, wherein the said nitrogenous hydrocarbons used have a C/N ratio of from 1 to 5.

Claim 4 (Currently Amended): A process as claimed in claim 1-or 2, wherein the said nitrogenous hydrocarbons used have a C/N ratio of from 5 to 7.

Claim 5 (Currently Amended): A process as claimed in one of claims 1 to 4 claim 1, wherein the said nitrogenous hydrocarbons used are one or more residues.

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Claim 6 Currently Amended): A process as claimed in one of claims 1 to 5 claim 1,

wherein water is introduced into the said flame reaction zone.

Claim 7 (Currently Amended): A process as claimed in one of claims 1 to 6 claim 1,

wherein one or more additional essentially inert-behaving further feed gas constituents are

introduced into said flame reaction zone. the flame.

Claim 8 (Currently Amended): A process as claimed in claim 7, wherein the said

essentially inert-behaving further feed gas constituents comprise carbon oxides and/or

hydrogen obtained from the said cleavage gas.

Claim 9 (Currently Amended): A process as claimed in one of claims 1 to 8 claim 1,

wherein a nitrogen oxide containing said gas comprising nitrogen oxide is introduced into the

said flame reaction zone.

Claim 10 (Currently Amended): A process as claimed in one of claims 1 to 9 claim

1, wherein the said nitrogenous hydrocarbons or said hydrocarbon mixture mixtures used are

<u>are/is</u> introduced in liquid form into the <u>said</u> flame reaction zone.

Claim 11 (Currently Amended): A process as claimed in claim 10, wherein the said

nitrogenous hydrocarbons used are atomized to form liquid droplets having a mean particle

diameter of <100 µm.

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Claim 12 (Currently Amended): A process as claimed in claim 10-or 11, wherein the said nitrogenous hydrocarbons or said hydrocarbon mixture is/are mixtures used are introduced as an aqueous emulsion into the said flame reaction zone.

Claim 13 (Currently Amended): A process as claimed in claim 12, wherein the said aqueous emulsion used is atomized to form liquid droplets having a particle diameter of <100 µm.

Claim 14 (Currently Amended): A process as claimed in one of claims 1 to 9 claim

1, wherein the said nitrogenous hydrocarbons used are introduced in the gaseous state into the said flame reaction zone.

Claim 15 (Currently Amended): A process as claimed in claim 14, wherein the said gaseous nitrogenous hydrocarbons are premixed with at least a part of the feed gas constituents selected from the group consisting of said oxygen-containing gas, said ammonia, the nitrogen oxide containing said gas comprising nitrogen oxide, said water and the said essentially inert-behaving feed gas constituents, and the resultant gas mixture is introduced into the said flame reaction zone.

Claim 16 (Currently Amended): A process as claimed in one of claims 1 to 15 claim

1, wherein turbulent flow prevails in the said reaction zones.

Claim 17 (Currently Amended): A process as claimed in one of claims 1 to 16 claim

1, wherein the resultant cleavage gas comprises at least the constituents hydrogen cyanide,

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earbon oxides, hydrogen, water, ammonia, nitrogen and light hydrocarbons and the separation of the resultant said cleavage gas comprises the steps:

- (i) cooling the said cleavage gas to a temperature <300°C;
- (ii) removing <u>said</u> ammonia as ammonium sulfate or ammonium phosphate by gas scrubbing, with <u>to obtain</u> an ammonia-depleted cleavage gas <u>being obtained</u>;
- (iii) removing <u>said</u> hydrogen cyanide as aqueous hydrogen cyanide solution[[,]] <u>to</u>
 <u>obtain</u> a hydrogen cyanide-depleted and ammonia-depleted residual cleavage gas <u>being</u>
 <u>obtained</u>;
- (iv) recovering hydrogen cyanide from the said aqueous hydrogen cyanide solution by distillation; and
- (v) where appropriate, partially recirculating the said residual cleavage gas to the said flame reaction zone.